



## GEOHERMAL WELL DESIGN

**Abdirasak Omar Moumin**

Ministry of Energy and Natural Resources

P.O. Box 10010

Djibouti

DJIBOUTI

*abdirasak@hotmail.fr*

### ABSTRACT

This report describes the geothermal well design for the future 4 wells in the Lava Lake area in Fiale Caldera in Djibouti. Various geophysical studies in the framework of different projects have confirmed the presence of a magmatic heat source potentially useful for the production of geothermal energy. The present work includes: the casing design, the wellhead pressure estimate, and cementing of the casings to prevent contamination of fresh water and maintain well integrity during exploitation. An Excel based programme was developed for the casing design. Also, the Viking engineering programme calculated the reduced collapse resistance and assisted the Excel programme. The criteria for the casing design were as follows: preliminary selection based on burst and collapse pressure, selection based on tension, and finally the biaxial correction. Since the reservoir pressures and temperatures of Wells AA, AB, AC and AD are not known, the reservoir pressure and temperature of Well Asal 5 were used to design the 4 wells and it is expected that the same casing string design will be used.

### 1. INTRODUCTION

The formation pressures, geology, hole depth, formation temperature and other factors are important for the final selection of casing grades and weights of a geothermal well. The casing design process consists of selecting the casing sizes, weight, grades and setting depths. This is done by calculating the burst, collapse, and axial loads affecting the casing during drilling of the well and also while the well is in production. Other factors such as corrosion must also be taken into account. The casing design is of utmost importance for the success of the well. The cost of the casing constitutes a considerable part of the total cost of the well, approximately 20%.

The first wells, in total six (Asal 1, 2, 3, 4, 5 and 6), were drilled in 1975 and 1987/1988 in the Lake Asal area to depths of 1316-2105 m, with temperatures up to 350°C (Elmi, 2005). Asal 5 will be used as a reference for designing the new wells AA, AB, AC and AD. The hydrostatic pressure profile for Asal 5 can be seen in APPENDIX III. The lithology from Asal 5 is better than what was expected for the Lava Lake in Fiale area. Asal 5 was drilled in the Inner Rift, about 1 km west of Lava Lake. The drilling of Well Asal 5 started on 7<sup>th</sup> January 1988 and finished on March 3, 1988. The final depth is 2,105 m and the temperature at the bottom is 350°C. It is unproductive and penetrates both cold and hot formations. In March 1988, Dr. Kristjan Saemundsson made a geological survey in the Asal Field, where he indicated that Well Asal 5 was not correctly sited, as it would be about 700-1000 m from the

geothermal upflow zone (Saemundsson, 1988). In June 1988, a resistivity survey using the TEM method (Transient Electromagnetics) was carried out in the "Inner Rift" (Árnason et al., 1988). The survey indicated the existence of an upflow zone of geothermal fluid under the Lava Lake, as had been predicted by Saemundsson (1988). These results show this area to be most promising for siting future exploratory wells.

## 2. WELL SITE GEOLOGY

The well design shall be based on a geological prognosis comprised of the expected stratigraphy and lithology. Geological conditions and fresh water aquifers are important factors for selecting the number of casing strings, casing setting depths and to select optimum drilling targets.

Wells AA, AB, AC, and AD will be sited in the Fiale area (Figure 1), specifically north of the Lava Lake about 70 km west of Djibouti city. The project area is estimated to be 2.5 km<sup>2</sup>. The sector is favoured because of its impressive faulting, massive magma deposition and active steam fumaroles on the surface. The Asal rift zone is dominated by very recent volcanic rocks and is characterized by a diverging plate boundary and continuous microseismic earthquakes. The last volcanic eruption took place in 1978 at Ardoukoba, southeast of Lake Asal. From 1975 to 1988 studies of the area were conducted. They proved that there is a heat source (350°C) in the area and that the fluids are highly saline (Virkir-Orkint, 1990). The Asal area is between Ghoubbet El Kharab and Lake Asal. The Fiale area is the southeast part of the Inner Rift. The Lava Lake is a circular depression in the centre of the Fiale area (REI, 2008). Djibouti is located where three major extensional structures, the Red sea, the East African Rift and the Gulf of Aden, meet and form the Afar Depression (Varet, 1973; Stieltjies, 1976).

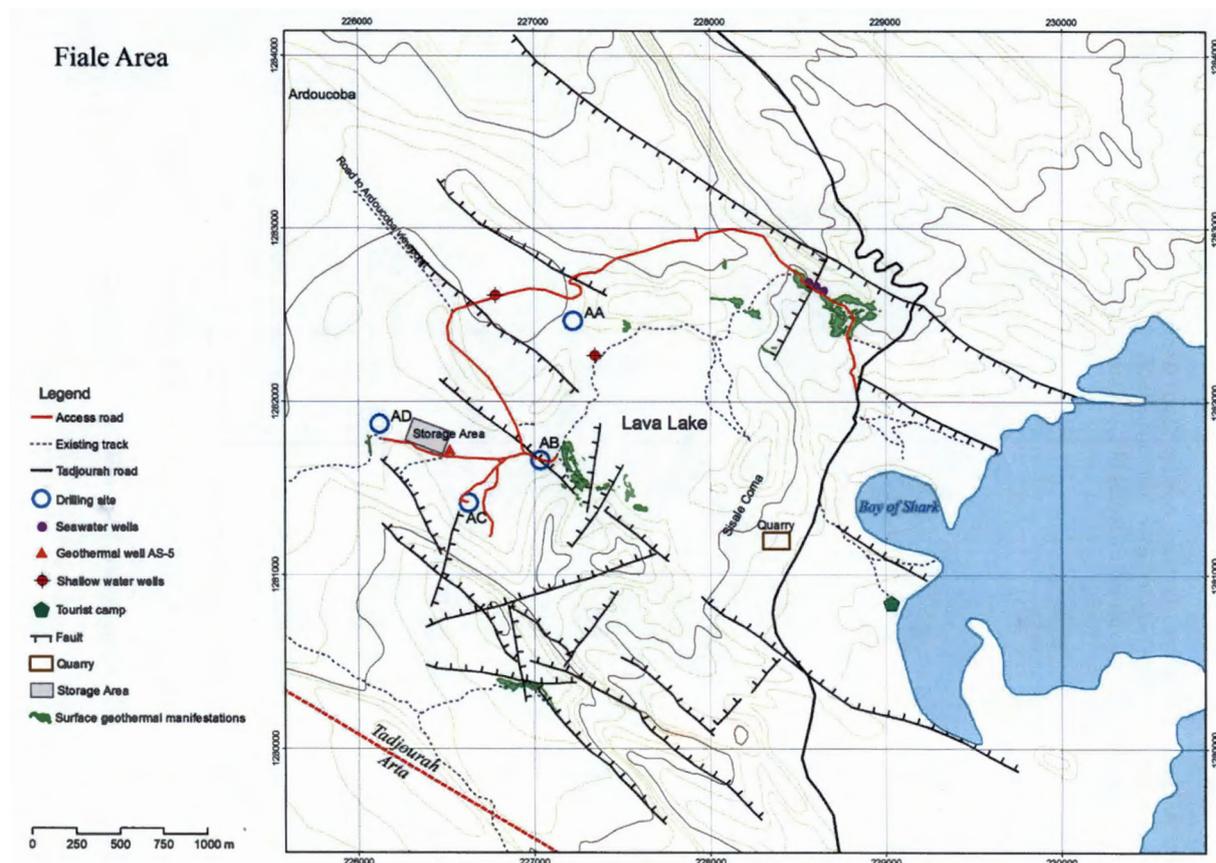


FIGURE 1: Map of Fiale area (REI, 2008)

The area could be impermeable. Significant fractures and faults are under the Lava Lake and it is a geological anomaly that should be protected. Therefore, the wells will not be drilled directly above the Lava Lake. To cut major faults, the technique of directional drilling will be used. The tectonic map is important for siting the wells and for targeting the faults.

**2.1 Lithological logs**

As already mentioned, the lithology of Well Asal 5 is expected to be similar to that of the new drilling site. The Italian company Aquater (Aquater, 1989) made lithological studies of Well Asal 5 and, in doing so, collected cuttings every 5 m. The cuttings were studied using a binocular microscope. Thin sections of the cuttings were collected every 10 m or when necessary every 5 m. The thin sections were studied using a polarizing microscope. The stratigraphic series was reconstructed and the hydrothermal alteration paragenesis was studied. The lithological sequence is quite monotonous, and most of the encountered rock type can be classified in the following units: ferrobasalt, olivine basalt, tuff, trachy-basalt, dark trachyte, sand or slit, and claystone (Figure 2).

**2.2 Alteration zones**

The hydrothermal mineral assemblages presented in Well Asal 5 indicate high-temperature geothermal activity. Six hydrothermal alteration zones were established based on the progressive alteration of the rock (Figure 3). These zones are as follows (Khairah, 1989): unaltered zone; smectite zone (this zone indicates a temperature range of up to 200°C); mixed layer clay zone (this zone is found at a

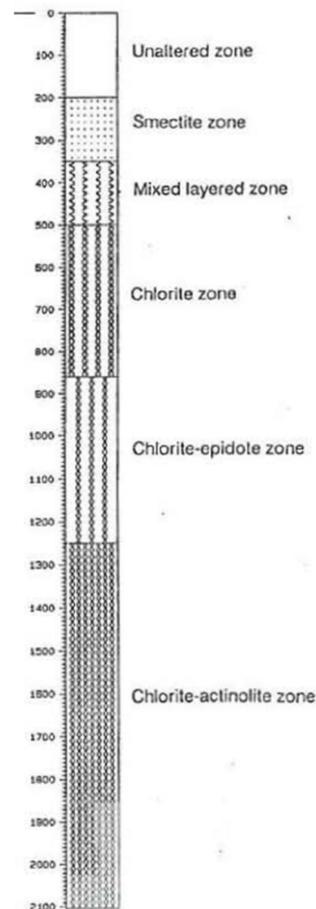
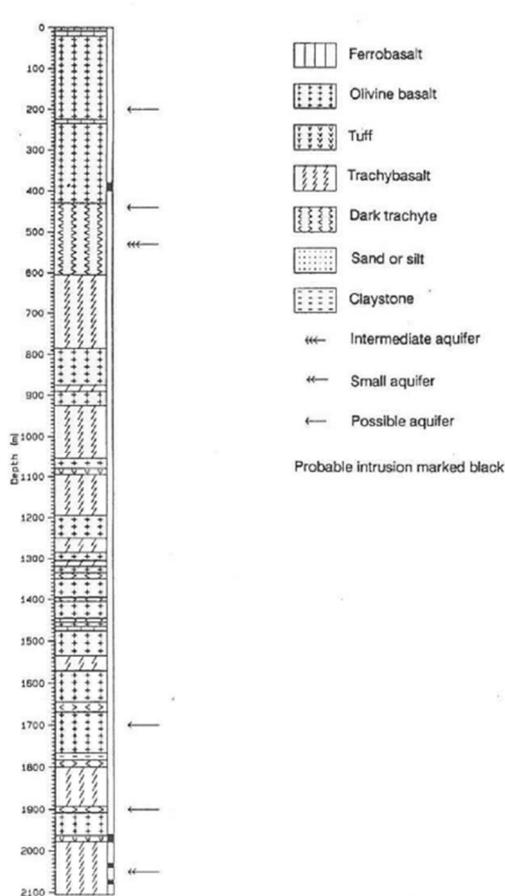


FIGURE 2: Lithological sequence expected for the Lava Lake in the Fiale area

FIGURE 3: Alteration zones for the Lava Lake in the Fiale area

temperature range of about 200-230°C); chlorite zone (the zone measures a temperature range of about 230-240°C); chlorite-epidote zone (this zone falls in the temperature range of 230-280°C); and chlorite-actinolite zone (this zone is correlated with temperatures exceeding 280°C).

### 2.3 Temperature profiles

Well Asal 5 showed a sharp increase in temperature below 200 m b.s.l., with a maximum of about 180°C at 500 m. Between 500 and 1000 m depth, the rocks drastically cooled down with temperatures as low as 60-70°C. After 1000 m depth, the temperature increased rapidly, reaching more than 350°C at 2100 m (Figure 4). The significant inversion on the temperature profile of Well Asal 5 might be explained by the superficial underground flow toward Lake Asal which goes deeper in this well (Jalludin, 2010). For wellhead design purposes, the temperature in the part that penetrates the cold formations was reversed and a maximum temperature of 312°C at 2050 m was assumed (Figure 5). If, during drilling, temperatures exceed this temperature according to cutting samples and temperature readings, drilling should be halted and a flow test conducted.

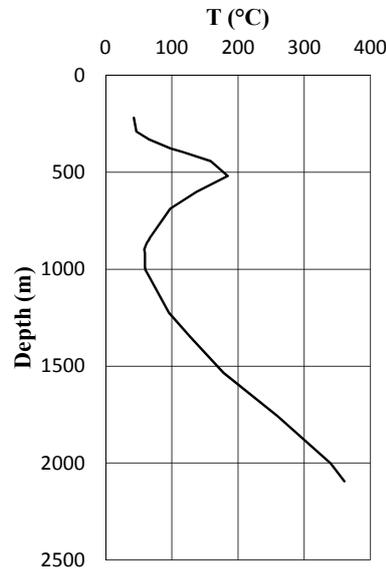


FIGURE 4: Temperature profile of Well Asal 5

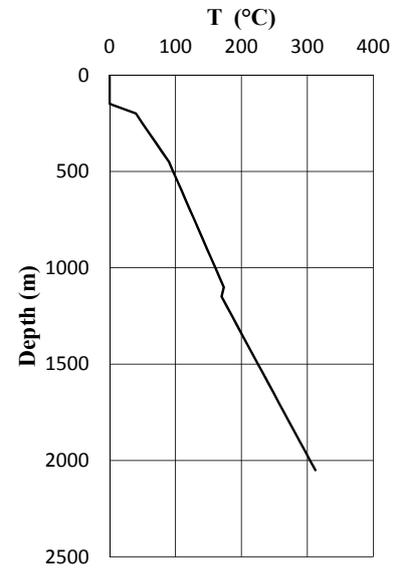


FIGURE 5: Expected temperature profile in the new wells

### 3. CASING DESIGN

The well design defines the desired final status of the well. Geothermal well designs and drilling practices are similar worldwide (Hosseini-Pourazad, 2005). The casing design is the same, whether the well is drilled vertically or directionally. Casings are designed to accomplish two different tasks. The first is to allow safe drilling of the well and to resist any force or conditions that are imposed upon it during drilling, without sustaining significant damage. The second is to meet the well's objectives without requiring a workover during the well's lifetime. Therefore, the main functions of the casing in any well are: to maintain hole integrity, to prevent contamination of near fresh water zones, to provide a suitable connection for the wellhead equipment and a hole of known diameters and depth to facilitate the running of test and completion equipment, to provide a conduit for well production, and to optimize well cost. Since pressure varies along each section of the hole, different casing sizes are employed; this arrangement gives a final tapered shape to the finished well. It is possible to run a casing string having the same outside diameters but with different thickness or strength properties. Thus, a heavy or high grade casing could be run along the section of the hole containing high pressures, or near the surface where tensile stresses are high. Multiple intervals of casing are successively placed within previous casings in geothermal wells. The typical casings used are:

*The conductor pipe* is the first casing to be put in place, and is often installed before the rig is mobilized. The conductor pipe can be excavated for or it can be driven with a hammer. It has the largest diameter and it is generally set at approximately 1-10 m below ground level. The conductor casing is used to seal off unconsolidated formations at shallow depths to prevent cave-ins.

*The surface casing* is the first casing string used after the conductor pipe. It supports the wellhead and BOP (Blow Out Preventer) equipment and other casings. The surface casing is used to seal off any fresh water zones and is generally set at approximately 50-200 m below ground level.

*The anchor casing* is run in deeper wells where kick tolerance or troublesome formations make it unsafe or undesirable to drill from the surface casing all the way to the production casing's setting depth in the hole section.

*The production casing* is the last casing string. It is run to isolate the producing zones, to provide reservoir fluid control, and to permit selective production in multi-zone production. It should be cemented to the top like the other casings. This is the string through which the well will be completed.

*A liner* is a casing string that does not reach the surface and is suspended from the inside of the previous casing string by a device known as a liner hanger or is allowed to stand on the bottom of the well. The liner hanger is usually attached to the second or third joint of the casing string. In liner completions, both the liner and the production casing act as the production string, but the liner can also be perforated and is then set in the production section, intended to keep the well from collapsing and remain permeable so that the geothermal fluid can flow into the well.

### 3.1 Casing materials

Other than the threaded connections used to connect together the individual joints of steel pipe for each casing string, various other items are required for the cementing operation; a reinforcement to the bottom joint of the casing and a connection for the wellhead may also be included in the casing string.

*Guide (float) shoe or casing shoe:* is attached to the bottom of the first casing joint and protects the casing bottom end from damage (during running of the casing) and the casing string from the impact associated with landing the casing on the bottom. To prevent the cement slurry from flowing back up the casing, the guide shoe has a non-return valve as a precaution.

*Liner hanger* allows the liner to be suspended from the previous casing; it is attached to the top of the liner. The choice of hangers will be limited to those compatible with the casing programme.

*Float collar* is normally installed one or two joints above the float- or guide shoe. The float collar prevents the cement being pumped into the casing/wellbore annulus from re-entering the casing after cementing operations and contains a non-return valve. When using an inner string, cementing the stab-in at the end of the cementing string is connected to the float collar.

*Scratchers* are devices attached to the outside of the casing, to remove the mud cake and break up gelled mud left by the drilling mud. They are sometimes run through the production zone.

*Centralisers* are installed on the casing string as it is run; a typical programme might be: 1 centraliser immediately above the shoe, 1 on every joint on the bottom 3 joints, 1 every joint through the production zone, 1 every 3 joints elsewhere. Their function is to reduce the friction between the casing string and the borehole and to centre the casing to ensure a cement sheath of sufficient thickness all around the casing. They are particularly required in deviated wells. Centralizer spacing depends on hole straightness and the clearance between the casing and bore.

### 3.2 Casing properties

Casing is usually specified by the following parameters: outside diameter, wall thickness, weight per unit length, type of connection, type of coupling, length joint, and grade of steel. The casings which

are most used have been standardised by the American Petroleum Institute (API). Appendix I lists the API specifications, standards and bulletins referred to in this report.

### 3.2.1 Casing size

TABLE 1: Drift mandrels

The size of the casing refers to the outside diameter (O.D.) of the main body of the tubular (not the connector). Casing sizes vary from 4.5" to 36" diameter. Tubulars with an O.D. of less than 4.5" are called tubing. API

Casing diameter (in)	Mandrel length		Mandrel diameter	
	(in)	(mm)	(in)	(mm)
< 9 5/8	6	152	ID-1/8	ID-3.18
9 5/8 to 13 5/8	12	305	ID-5/32	ID-3.97
13 3/8 and larger	12	305	ID-3/16	ID-4.76

ID: Inside diameter

recommended dimensions of drift mandrels, which are used to determine the pipes inner roundness, are as follows: the drift diameter (Table 1) is the maximum size of a drill bit that can safely be run through the casing.

### 3.2.2 Joint length

TABLE 2: Length range of a casing joint - API

The length of a joint of casing has been standardised and classified by the API (Table 2). The precise length of each joint has to be measured. The length is measured from the top of the connector to a

Range	Length		Average length	
	(feet)	(m)	(feet)	(m)
1	16-25	4.9-7.6	22	6.7
2	25-34	7.6-10.4	31	9.45
3	Over 34	Over 10.4	42	12.8

reference point on the pin at the other end of the casing joint. Casing is run most often in Range 3 lengths to reduce the number of connections in the string. Since casing is made up of single joints, Range 3 lengths can be handled easily by most rigs.

### 3.2.3 Casing weight

The weight per foot of the casing is representative of the wall thickness of the pipe. There are, for instance, three different weights of 20" casing; see the *Drilling data handbook* (Gabolde and Nguyen, 2006).

### 3.2.4 Connections

The casing is fabricated in joints and is delivered to the rig. The casing joints are joined together by threaded connections. They exist in a wide variety of threaded connections. In the API standard 5B, the connection between the joints is carried out by coupling; it (coupling or casing collar) is threaded internally (female) and is installed on one end of each joint before it is delivered to the rig. Contrary to coupling, the casing joints are threaded externally at either end. The standard types of API threaded and coupled connections are:

- Short thread connection (STC);
- Long thread connection (LTC); and
- Buttress thread connection (BTC).

### 3.2.5 Casing grade

API defines the characteristics of various steels and assigns letters to identify those grades (the chemical composition of the material); the number refers to the minimum yield strength of the material, e.g. N-80 casing has the minimum yield strength of 80000 psi and K-55 has the minimum yield strength of 55000 psi; refer to API specification 5CT for complete definitions. Table 3 shows the different grades of steel classified by API. Certain manufacturers produce non-API materials.

Both seamless and welded tubulars are used as casing although seamless casing is the most common type of casing and usually only H and J grades are welded.

TABLE 3: Tensile requirements for casing and tubing

Grades		H40	J55	K55	N80	L80	C90	C95	T95	P110
Properties		H40	J55	K55	N80	L80	C90	C95	T95	P110
Grades color codes		1 black	1 green	2 green	1 red	1 red 1 brown	1 purple	1 brown	1 silver	1 white
Min. yield strength	Bar	2760	3790	3790	5520	5520	6210	6550	6550	7580
	Psi	40000	55000	55000	80000	80000	90000	95000	95000	110000
Max. yield strength	Bar	5520	5520	5520	7580	6550	7240	7580	7580	9650
	Psi	80000	80000	80000	110000	95000	105000	110000	110000	140000
Min. ultimate tensile strength	Bar	4140	5170	6550	6890	6550	6890	7240	7240	8620
	Psi	60000	75000	95000	100000	95000	100000	105000	105000	125000

### 3.3 Safety factor

The exact values of loadings are difficult to determine; the safety factor is used to allow and to ensure that the rated performance of the casing is always greater than any expected load. Safety factors are arbitrary figures that have evolved with experience. Each operating company uses its own values for safety factors for specific situations. The minimum acceptable casing design factors (NZS, 1991) are:

- Internal yield (burst) design factors 1.5 -1.8;
- Collapse design factors 1.2;
- Tensile design factors 1.5 – 1.8; and
- Compressive factor 1.2.

### 3.4 Casing design criteria

Generally, the casing design process involves three distinct steps: The selection of the casing sizes and setting depths; the definition of the operational scenarios which will result in burst, collapse and axial loads being applied to the casing; and the calculation of the magnitude of these loads and selection of an appropriate weight and grade of casing. The load inside any particular string will differ from those inside the other strings. Each string of casing must be carefully designed to withstand the anticipated loads to which it will be exposed during installation, when drilling the next hole section, and when producing from the well.

Radial loads (burst and collapse) and axial (tensile and compressive) loads to which the casing will be exposed during the lifetime of the well will dictate the depth of the casing shoe. The casing design should be calculated using the true vertical depth. The majority of the equations used in this section have been extracted from Baker Hughes INTEQ (1995), BG Group (2001), and Heriot-Watt University (2010).

#### 3.4.1 Collapse

Collapse pressure originates from the column of mud used during drilling and the column of cement used to cement the casing in place. The collapse load at any point along the casing can be calculated from:

$$P_c = P_e - P_i \quad (1)$$

where  $P_c$  = Collapse pressure;

- $P_e$  = External pressure due to mud or cement; and  
 $P_i$  = Internal pressure due to mud, water or cement.

Before designing each casing string, it is important to define the hypotheses to be considered:

- While running casing and designing for the collapse pressure, the internal pressure is zero ( $P_i=0$ ) because the surface, anchor and production casings are assumed to be empty (full evacuation).
- At the surface we assume that the collapse pressure is zero ( $P_c = 0 = P_e$ ).
- At the shoe of each casing string, the maximum collapse pressure is calculated. The collapse pressure increases with depth, going from zero at surface to the maximum value at the shoe.

The equation for the collapse pressure while running the casing generally is as follows:

$$\begin{array}{l} \text{At surface} \qquad \qquad \qquad P_c = 0 \\ \text{At shoe} \qquad \qquad \qquad P_c = P_e = \rho \times g \times \text{CSD} \end{array} \quad (2)$$

- where
- $P_c$  = Collapse pressure;
  - $P_e$  = External pressure (due to drilling mud or other drilling fluid);
  - $g$  = Force of gravity;
  - CSD = Casing setting depth; and
  - $\rho$  = Density of drilling mud.

In *metric units*, the collapse pressure is given by:

$$P_c = \rho \times 0.0981 \times \text{CSD} \quad (3)$$

- where
- $P_c$  = Collapse pressure (bar);
  - CSD = Casing setting depth (m); and
  - $\rho$  = Density of current drilling mud (kg/l).

while in *imperial units*, the collapse pressure is given by:

$$P_c = \rho \times 0.052 \times \text{CSD} \quad (4)$$

- where
- $P_c$  = Collapse Pressure (psi);
  - CSD = Casing Setting Depth (feet);
  - $\rho$  = Density of current drilling mud (ppg).

After running the casing and when designing for the collapse pressure, the column of cement imposes the external pressure, and the casing is assumed to be full of water.

The density of fluid inside the casing is equal to 1 kg/l, hence:

$$P_e = \rho[\text{cement}] \times g \times \text{CSD} \quad (5)$$

$$P_i = \rho[\text{fluid inside the casing}] \times g \times \text{CSD} \quad (6)$$

$$\text{At shoe} \qquad P_c = [\rho[\text{cement}] - \rho[\text{fluid inside the casing}]] \times g \times \text{CSD} \quad (7)$$

$$\text{At surface} \qquad \qquad \qquad P = 0$$

The collapse pressure due to the mud column ( $P_i = 0$ , inside casing totally empty) is higher than the collapse pressure due to the cement column ( $P_i \neq 0$ , casing full of displacement fluid); that is why the collapse pressure due to the mud column is used for the design of the collapse resistance. Then the design factor, discussed in Section 3.3, is added.

### 3.4.2 Burst

The burst pressure design must ensure that the pressure inside the casing does not exceed the casing burst pressure limit. The top section of each casing string and wellhead shall be designed to resist the pressure and temperature conditions. The pressures at the surface and at the casing shoe are calculated by the equation defined below:

$$P_b = P_i - P_e \quad (8)$$

When designing for the burst pressure, to optimize the casing's resistance, it is assumed that at the surface the internal pressure is due to the hydrostatic pressure minus the weight of the gas. The external pressure is assumed to be  $P_e = 0$ .

*Burst at surface:*

$$P_e = 0 \quad (9)$$

$$P_i = P_h - \text{NHTD} \times \rho_2 \times 0.0981 = P_b \quad (10)$$

The hydrostatic pressure is given by the following equation:

$$P_h = \text{NHTD} \times \rho_1 \times 0.0981 \quad (11)$$

where  $P_b$  = Burst pressure at surface (bar);  
 $P_i$  = Internal pressure at surface (bar);  
 $P_e$  = External pressure at surface (bar);  
 $P_h$  = Hydrostatic pressure at NHTD (bar);  
 $\rho_1$  = Density of saturated liquid;  
 $\rho_2$  = Gas density at NHTD; and  
 NHTD = Next hole total depth (m).

For more details, see Section 6 where the hydrostatic pressure is calculated for every 50 m.

*Burst at shoe:*

$$P_e = \text{CSD} \times 0.105 \quad (12)$$

The gradient of salt water is 0.105 bar/m or 0.465 psi/ft.

$$P_i = P_p + \rho_c \times L_c \times 0.0981 + L_w \times \rho_w \times 0.0981 \quad (13)$$

$$P_b = P_i - P_e \quad (14)$$

where  $P_b$  = Burst pressure at shoe (bar);  
 $P_i$  = Internal pressure at shoe (bar);  
 $P_e$  = External pressure at shoe (bar);  
 $P_p$  = Applied pressure pumping (bar);  
 $\rho_c$  = Cement slurry density (kg/l);  
 $\rho_w$  = Density of displacement fluid (kg/l);  
 $L_c$  = Height of cement column inside casing (m); and  
 $L_w$  = Height of water column inside casing (m).

### 3.4.3 Axial loads: tension load

The axial load that may be exerted on the casing string is the tension and compression that occur under the following conditions (Figure 6): the tension is due to the weight of the casing and the cooling of the well, and the compressive loads are due to thermal expansion during heating-up of the well.

Casings are mostly in tension except for conductor pipes. Tension loads are determined by: the forces due to the buoyed weight, the bending force in deviated wells, the shock load and the force due to pressure testing. The design factor for all axial tensile and compressive loading shall not be less than 1.2 (NZS, 1991). If the yield strength of casing is exceeded during running and cementing of the casing, then casing failure is likely.

*Calculation of buoyed weight:*

The weight of casing in air is given by:

$$W_a = W_p \times \text{CSD} \quad (15)$$

where  $W_p$  = Nominal unit weight of casing (lb/ft); and  
 $W_a$  = Weight air (lb).

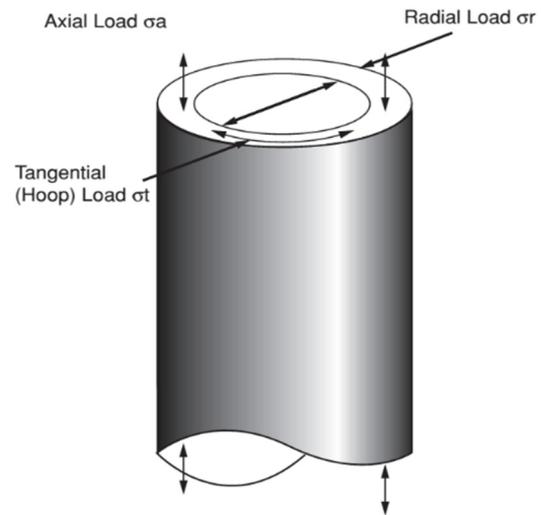


FIGURE 6: Casing loads

Therefore, the buoyant weight of casing is given by:

$$W_b = W_a \times \text{BF} \quad (16)$$

$$\text{BF (Buoyancy factor)} = 1 - \frac{\rho}{\rho_s} \quad (17)$$

where  $\rho_s$  = Steel density (7.85 kg/l);  
 $\rho$  = Density of fluid (fluid displacement or mud or cement) (kg/l); and  
 $W_b$  = Buoyant weight (lb).

Hence

$$\text{Buoyancy force} = W_a(1 - \text{BF}) \quad (18)$$

*Calculation of buoyed weight in different liquids (inside and annular):*

Here, the buoyant weight is determined by using the buoyancy factor from the following equation:

$$\text{BF} = \frac{\left[1 - \frac{\rho_e}{\rho_s}\right] - \frac{\text{ID}^2}{\text{OD}^2} \times \left[1 - \frac{\rho_i}{\rho_s}\right]}{1 - \frac{\text{ID}^2}{\text{OD}^2}} \quad (19)$$

where ID = Inside diameter (in);  
 OD = Outside diameter (in);  
 $\rho_i$  = Density of fluid inside casing (kg/l); and  
 $\rho_e$  = Density of fluid outside casing (kg/l).

When the cement is inside the casing, the tensile force at the surface from the casing weight (buoyant weight) is at its maximum value and the minimum value of the tensile force at the surface from the casing weight is attained when the entire volume of cement is displaced outside the casing.

*Bending force:*

Bending force arises if casing is run in deviated wells or in wells with severe dogleg. In the deviated wells, the bends must be considered. The bending force can be computed from the following:

$$B_f = 63 \times W_p \times \text{OD} \times \theta \quad (20)$$

where OD = Outside diameter (in);  
 $\theta$  = Dogleg severity, degrees/100 ft;

$W_p$  = Nominal unit weight of casing (lb/ft); and  
 $B_f$  = Bending force (lb).

*Shock loads:*

The casing string experiences shock loads when it is decelerated or accelerated while setting or unsetting the casing slips. The shock load is given by:

$$\text{Shock load} = 3200 \times W_p \quad (21)$$

To recap, the preliminary casing selection is based on burst and collapse, and the safety factor in tension during pressure testing must be more than 1.5 – 1.8; it is given by the relationship below. The casing should be tested to the maximum pressure for which it has been designed.

$$\text{Safety Factor in tension} = \frac{\text{Yield Strength}}{\text{Total Tensile loads}} \quad (22)$$

$$\text{Total tensile loads} = W_b + B_f + \text{Shock load} + \text{Force due to pressure testing} \quad (23)$$

$$\text{Force due to pressure testing} = \frac{\pi}{4} \times \text{ID}^2 \times \text{testing pressure} \quad (24)$$

where Testing pressure = 60% (depends on the company involved)  $\times$  Burst pressure.

*Axial loading applied to the liner:*

The perforated liner in the production section of the well is not cemented and is not supported or constrained. Therefore, the extreme compressive stress, due to the thermal expansion and bending forces concerning the perforated liner, is given by:

$$F_{ec} = L_z \times W_p \times g \left[ \left[ \frac{1}{A_p} \right] + \left[ \frac{\text{OD} \times e}{L_p} \right] \right] \quad (25)$$

where  $F_{ec}$  = Extreme compressive stress (N);  
 $L_z$  = Length of the liner (m);  
 $W_p$  = Nominal weight of casing (kg/m);  
 $g$  = Acceleration due to gravity ( $\text{m s}^{-2}$ );  
 $A_p$  = Cross-section area of pipe ( $\text{m}^2$ );  
 $\text{OD}$  = Outside diameter (m);  
 $e$  = Eccentricity (actual hole diameter minus OD) (m); and  
 $L_p$  = Net moment of inertia of the pipe section, allowing for perforation ( $\text{kg m}^2$ ).

After the well has been completed, the tensile axial load in the top section of the casing, below the wellhead, applied by the fluid in the well is:

$$F_w = \frac{\pi}{4} P_w \text{ID}^2 \quad (26)$$

where  $F_w$  = Lifting force due to wellhead pressure (N);  
 $P_w$  = Maximum wellhead pressure (Pa); and  
 $\text{ID}$  = Inside diameter of production casing ( $\text{m}^2$ ).

### 3.4.4 Axial loads: compression

The compressive loads due to thermal expansion during heating-up of the well when the casing is constrained both longitudinally and laterally by cement is:

$$F_c = C_t \times [T_2 - T_1] \times A_p \quad (27)$$

where  $F_c$  = Compressive loads (N);

- $C_t$  =  $E \times a$ , thermal stress constant for casing steel (MPa/°C);  
 $T_2$  = Maximum expected temperature (°C);  
 $T_1$  = Neutral temperature (temperature at time cement is set (°C);  
 $A_p$  = Cross-section area of pipe (m<sup>2</sup>);  
 $E$  = Modulus of elasticity; and  
 $a$  = Coefficient of linear thermal expansion.

Casing string design shall allow for the changes in casing properties at elevated temperatures, as shown in Table 4. The modulus of elasticity can be assumed to be constant over the temperature range; the value is  $200 \times 10^6$  MPa. The coefficient of linear, thermal expansion should be taken as  $12 \times 10^{-6}/^\circ\text{C}$ . Normally the coefficient of linear, thermal expansion is not constant, particularly at low temperature and pressures, and must be determined by reference to the steam tables. Therefore, the thermal stress constant for casing steel is:  $C_t = 2.4$  MPa/°C.

TABLE 4: Temperature effects (NZS) on casing properties (K-55)

	Temperature (°C)			
	20 (°C)	100 (°C)	200 (°C)	300 (°C)
API yield strength	1	0.95	0.95	0.95
Tensile strength	1	0.97	1.02	1.07
Modulus of elasticity	208	208	200	192

### 3.4.5 API rated capacity of casing

The API bulletin 5C3 defines four formulas for calculating the collapse resistance of casings (Rabia, 1987). The API collapse formulas predict acceptable minimum collapse values, not average values. They are determined by yield strength of axial stress (see Section 3.6.5) and OD/t. They are given by the following equations:

The theoretical *elastic collapse pressure*,  $P_c$ , may be determined from the following equation in imperial units:

$$P_c = \frac{46.978 \times 10^6}{\left[ \frac{OD}{t} \left[ \frac{OD}{t} - 1 \right]^2 \right]} \quad (28)$$

where  $P_c$  = Elastic pressure (psi);  
 OD = Outside diameter (in); and  
 t = Wall thickness (in).

And in metric units:

$$P_c = \frac{3.304 \times 10^6}{\left[ \frac{OD}{t} \left[ \frac{OD}{t} - 1 \right]^2 \right]} \quad (29)$$

The elastic collapse pressure equation (Equation 28) is applicable where the following relationship is satisfied:

$$\frac{OD}{t} \geq \frac{2 + \frac{B}{A}}{3 \times \frac{B}{A}} \quad (30)$$

where

$$A = 2.8762 + 0.10679 \times 10^{-5} Y_p + 0.21301 \times 10^{-10} Y_p^2 - 0.53132 \times 10^{-16} Y_p^3 \quad (31)$$

$$B = 0.026233 + 0.50609 \times 10^{-6} Y_p \quad (32)$$

and  $Y_p$  = Minimum yield strength of the casing (psi).

The *transition collapse pressure* ( $P_t$ ) is given by:

$$P_t = Y_p \times \left[ \frac{C}{\frac{OD}{t}} - D \right] \quad (33)$$

where C and D are constants given by the following relationship:

$$C = \frac{46.95 \times 10^6 \left[ \frac{3\frac{B}{A}}{2+\frac{B}{A}} \right]^3}{Y_p \left[ \frac{3\frac{B}{A}}{2+\frac{B}{A}} \right] \left[ \frac{3\frac{B}{A}}{2+\frac{B}{A}} \right]^2} \quad (34)$$

$$D = \frac{CB}{A} \quad (35)$$

Equation 33 is applicable if:

$$\frac{Y_p[A - C]}{E + Y_p[B - D]} \leq \frac{OD}{t} \leq \frac{2 + \frac{B}{A}}{3\frac{B}{A}} \quad (36)$$

where

$$E = -465.93 + 0.030867Y_p - 0.10483 \times 10^{-10}Y_p^2 + 0.36989 \times 10^{-13}Y_p^3 \quad (37)$$

The *plastic collapse pressure* may be calculated from the following equation:

$$P_p = Y_p \left[ \frac{A}{\frac{OD}{t}} - B \right] - E \quad (38)$$

Equation 38 is applicable if the following relationship is verified:

$$\frac{[A - 2]^2 + 8 \left[ B + \frac{E}{Y_p} \right]^{1/2} + [A - 2]}{2 \left[ B + \frac{E}{Y_p} \right]} \leq \frac{OD}{t} \leq \frac{Y_p[A - C]}{E + Y_p[B - D]} \quad (39)$$

The *yield strength collapse pressure*,  $P_y$ , is calculated by:

$$P_y = 2Y_p \left[ \frac{\frac{OD}{t} - 1}{\left( \frac{OD}{t} \right)^2} \right] \quad (40)$$

The range of OD/t is:

$$\frac{OD}{t} \leq \frac{[A - 2]^2 + \left[ B + \frac{E}{Y_p} \right]^{1/2} + [A - 2]}{2 \left[ B + \frac{E}{Y_p} \right]} \quad (41)$$

### 3.4.6 Biaxial loads

The radial stress is often negligible compared to the axial and tangential stresses. The manufacturer provides the collapse resistance for casing under zero axial load. Under field conditions, this is never the case. Considering the axial stress, the new yield strength is given by:

$$Y_{pa} = \left[ \sqrt{1 - 0.75 \times \left[ \frac{S_a}{Y_p} \right]^2} - 0.5 \times \frac{S_a}{Y_p} \right] Y_p \quad (42)$$

where  $Y_{pa}$  = Yield strength considering axial stress, psi or MPa;  
 $Y_p$  = Minimum yield strength of the casing, psi or MPa; and  
 $S_a$  = Axial stress, psi or MPa.

$$S_a = \frac{\text{Axial load(lb)}}{\text{Cross section area(in}^2\text{)}} \quad (43)$$

The result from Equation 42 will be used for calculating burst and collapse (see above). The minimum burst resistance of the casing is calculated by using Barlow's equation:

$$P = 0.875 \times \left[ \frac{2 \times Y_{pa} \times t}{OD} \right] \quad (44)$$

And the minimum collapse resistance is calculated by the following steps:

- Calculate the axial stress ( $S_a$ ) at the section of casing under consideration;
- Determine (Equation 42) the yield strength considering the axial stress,  $Y_{pa}$ ;
- Calculate the ratio OD/t;
- Using Equations 31, 32, 34, 35 and 37, calculate the constants A, B, C, D and E and determine the range for which OD/t is applicable (Equations 30, 36, 39 and 41); and
- Determine the appropriate equation for calculating the reduced collapse resistance from OD/t.

Viking Engineering, LG, has developed an Excel based programme to calculate collapse resistance. The input data are: OD, pipe weight per foot, grade, the yield strength considering the axial stress ( $Y_{pa}$ ), and t (thickness). The output of the programme is A, B, C, D, F (in the programme, C=F and D = G), and the collapse resistance.

### 3.4.7 Triaxial loads

In the most critical case, one needs to take into consideration triaxial stress analysis. To calculate it, the radial, tangential, and axial stresses need to be calculated. Often, the triaxial stress analysis is not used but, in reality, the casing string is submitted to triaxial loading. In the casing design of wells AA, AB, AC and AD, we do not consider the triaxial stress analysis.

## 4. CASING DESIGN PROGRAMME FOR WELLS AA, AB, AC, AD

In this part, the casing design for wells Asal A, Asal B, Asal C and Asal D are presented. To do this, an Excel based programme was used as well as the Viking Engineering programme, which was used to calculate the reduced collapse resistance.

### *Step 1: Preliminary selection of weight and grade, based on burst and collapse pressure*

The program calculates the burst pressure at the shoe and at the surface, as well as the collapse pressure at the shoe and at the surface for each casing string. The input data for the programme is namely the casing setting depth, the mud programme, the hydrostatic pressure, the temperature and the gas density.

### *Step 2: Selection based on tension*

After step 1, the burst and collapse requirements are known, and the weight and grade of the casing are selected. Therefore, the tension can be calculated. The input data for the programme is the specifications of the casing string given by the manufacturer. The programme determines the total

tensional load, the safety factor for the casing in tension, and the safety factor in tension during pressure testing. If the safety factor is more than 1.6, the preliminary selection grade and weight is approved. Otherwise, replace and choose heavier casing string and check the calculation again.

*Step 3: Viking engineering programme; Axial stress, yield strength of axial stress equivalent grade and reduced collapse pressure*

The last step determines the effect of tensile load on collapse resistance, yield strength and the burst resistance. This calculation is done by the Viking programme. The input data is given by the principal programme.

**4.1 Hole and casing sizes**

The first decision required is the diameter of the production casing; then the other casing strings are chosen according to the availability of standard casing and bit sizes, rig equipment or other factors that give the desired clearances (Devereux, 1998). The considerations in selecting the diameter of the production casing are: the desired size of the production or test tube, and the requirements for logging or for gathering information from the well. Worldwide, in most high-temperature wells two basic designs are used: regular diameter wells with a production casing of 9 5/8" and a slotted liner of 7"; and large diameter wells with a casing of 13 3/8" and a slotted liner of 9 5/8".

In the environmental impact assessment report (Meinken and Schülein, 2012), it was decided to drill wells AA, AB, AC and AD with a 9 5/8" production casing. Figure 7 shows the sequence of casing and bit sizes planned for the 4 wells.

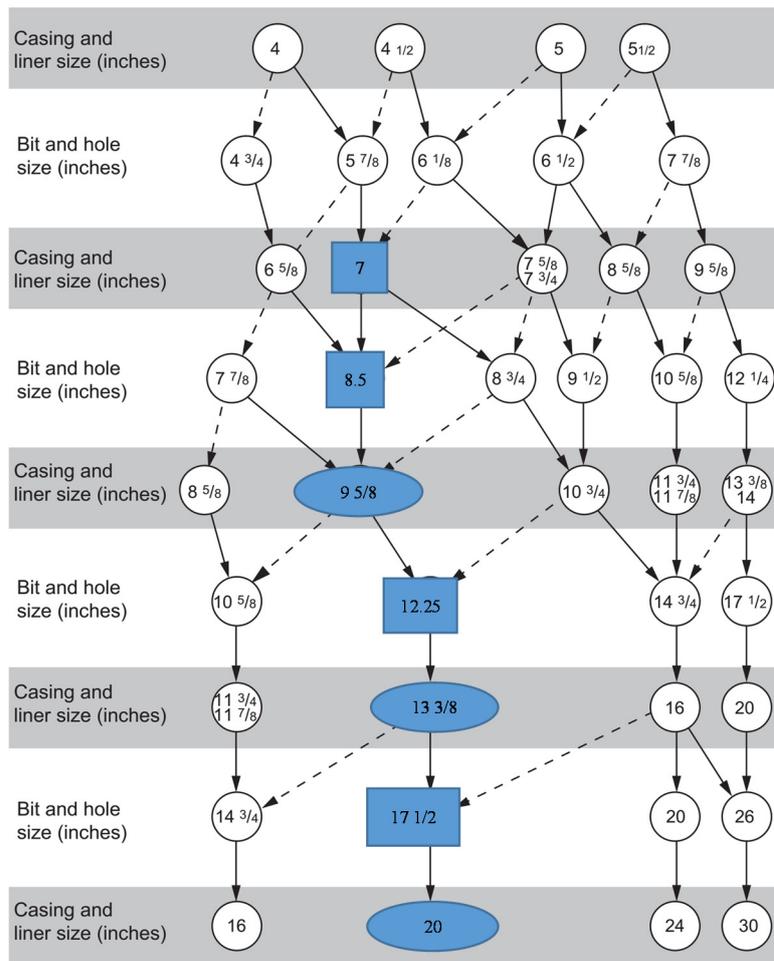


FIGURE 7: Casing programme for Wells in the Fiale area  
Casing sequence (blue ,ellipse)), bit sizes (blue, box).

**4.2 Casing setting depth**

When designing the casing setting depths, several different factors need to be taken into account: geological information, lithological column, pore pressure gradients and fracture gradients of the formations to be penetrated, and any other available data. Often, in high-temperature areas the casing strings are: conductor casing, surface casing, anchor casing and production casing. In the open section of the hole, there is also the liner which can be hung from the production casing or set on the bottom of the well.

The New Zealand standard method was used for designing the casing setting depths for Wells AA, AB, AC and AD. It is a method for determining the minimum casing depth for high-temperature geothermal wells. As already mentioned, the presence of a strong circulation of cold sea water close to Well Asal 5 between 500 and 1100 m depth could affect the production zone planned for the 4 wells. So, to protect the production zone, the production casing depth is set at 1210 m and the surface and anchor casing depths are deduced using the New Zealand standard method. The drilling programme for Wells AA, AB, AC and AD is summarized in Table 5.

TABLE 5: Drilling programme: Wells AA, AB, AC and AD

	Surface Casing	Anchor Casing	Production Casing	Liner
Nominal size (OD):				
inches	20	13.375	9.625	7
mm	508	339.73	244.48	177.8
Diameter hole/bit:				
inches	26	17.5	12.25	8.5
mm	660.4	444.5	311.15	215.9
Casing setting depth:				
m	160	480	1210	2050
feet	525	1575	3970	6726
Drilling fluid:	Foam	Sea water based mud	Sea water based mud	Sea water/aerated
Density drilling fluid:				
kg/l	0.6	1.05	1.05	NA
ppg	5.01	8.76	8.76	NA

#### 4.3 Selection of grade and weight

With an Excel worksheet, the burst and the collapse loads were calculated to select an appropriate weight and grade for surface, anchor and production casings. It is assumed that the casings are totally empty due to losses of drilling fluid and the applied pumping pressure is neglected. For the design, the effects of temperature on the casing properties (discussed in Section 3.4.4) were not considered. Tables 6 and 7 give the results of the burst and collapse calculations for each casing. The liner does not undergo burst or collapse loads because it is perforated.

The burst and collapse resistance of the available grade in API must be higher than the collapse and burst loads. The appropriate grade and weight for Wells AA, AB, AC and AD are:

- a. Surface casing: 20" 94.0 lb/ft K55;
- b. Anchor casing: 13.375" 54.50 lb/ft K55; and
- c. Production casing: 9.625" 40 lb/ft K55.

It is possible to use the grade and weight above but, to be on the safe side, because the anchor and production casings are set rather deep and to anticipate added pressures due to cementing pumping pressures, 68 lb/ft for the anchor casing and 47 lb/ft for the production casing were selected. The liner is perforated and, therefore, there is no burst or collapse pressure acting on it. A 7" 26.0 lb/ft perforated liner is sufficient, using Equation 27. Using Halliburton eRedbook, a drawing of the wellbore for the wells was made (Figure 8). For each casing, the collapse pressure was drawn between 0 at the surface and the maximum value at the casing setting depth. The collapse and burst resistance values were plotted as vertical lines, as shown in Figures 9, 10 and 11.

TABLE 6: Results of burst pressure calculations for each casing

<b>Surface casing</b>				
CSD	160.00	m	524.93	ft
Next hole total depth	480.00	m	1574.80	ft
Height of cement column inside casing	76.57	m	251.20	ft
Height of water column inside casing	83.43	m	273.73	ft
Density of current drilling mud	0.60	kg/l	5.01	ppg
Density of displacement fluid	1.00	kg/l	8.35	ppg
Density of cement (class G)	1.90	kg/l	15.86	ppg
Gas density at NHTD	0.0005	kg/l	0.00442	ppg
Gradient of salt-saturation	0.105	bar/m	0.465	psi/m
Force of gravity	0.0981			
Applied pumping pressure	14.13	bar	204.89	psi
Hydrostatic pressure at NHTD	29.00	bar	420.62	psi
<i>Burst at surface</i>	28.98	bar	420.25	psi
Burst at surface by safety factor 1.5	43.46	bar	630.38	psi
Pe at surface	0	bar	0	psi
Pi at surface	28.98	bar	420.25	psi
<i>Burst at shoe</i>	19.78	bar	286.92	psi
Burst at shoe by safety factor	29.67	bar	430.39	psi
Pe at shoe	16.80	bar	243.67	psi
Pi at shoe	36.58	bar	530.59	psi
Calculation of height of water and cement inside the casing				
Capacity of cylinder 20"	202.70	l/m		
Capacity of surface casing 20"	32432	l	32.43	m3
Volume of slurry	38800	l	38.80	m3
60% freshwater	23280	l	23.28	m3
40% cement (class G)	15520	l	15.52	m3
<b>Anchor casing</b>				
CSD	480	m	1574.80	ft
Next hole total depth	1210	m	3969.82	ft
Height of cement column inside casing	218.33	m	716.31	ft
Height of water column inside casing	261.67	m	858.49	ft
Density of current drilling mud	1.05	kg/l	8.76	ppg
Gas density at NHTD	0.005	kg/l	0.04173	ppg
Applied pumping pressure	42.38	bar	614.67	psi
Hydrostatic pressure at NHTD	92.00	bar	1334.37	psi
<i>Burst at surface</i>	91.41	bar	1325.76	psi
Burst at surface by safety factor 1.5	137.11	bar	1988.64	psi
Pe at surface	0.00	bar	0.00	psi
Pi at surface	91.41	bar	1325.76	psi
<i>Burst at shoe</i>	58.34	bar	846.22	psi
Burst at shoe by safety factor	87.52	bar	1269.33	psi
Pe at shoe	50.40	bar	731.00	psi
Pi at shoe	108.74	bar	1577.22	psi
Calculated height of water and cement inside the casing				
Capacity of cylinder 13.375"	90.64	l/m		
Capacity of anchor casing 13.375"	43507.20	l	43.51	m3
Volume of slurry	49474.00	l	49.47	m3
60% freshwater	29684.40	l	29.68	m3
40% cement (class G)	19789.60	l	19.79	m3

TABLE 6 cont.: Results of burst pressure calculations for each casing

<b>Production casing</b>				
CSD	1210	m	3969.82	ft
Next hole total depth	2050	m	6725.72	ft
Height of cement column inside casing	454.16	m	1490.04	ft
Height of water column inside casing	755.84	m	2479.78	ft
Density of current drilling mud	1.05	kg/l	8.76	ppg
Gas density at NHTD	0.0565	kg/l	0.47150	ppg
Applied pumping pressure	106.83	bar	1549.48	psi
Hydrostatic pressure at NHTD	158.20	bar	2294.55	psi
<i>Burst at surface</i>	146.84	bar	2129.75	psi
Burst at surface by safety factor 1.5	220.26	bar	3194.62	psi
Pe at surface	0	bar	0	psi
Pi at surface	146.84	bar	2129.75	psi
<i>Burst at shoe</i>	138.58	bar	2009.96	psi
Burst at shoe by safety factor	207.87	bar	3014.94	psi
Pe at shoe	127.05	bar	1842.73	psi
Pi at shoe	265.63	bar	3852.70	psi
Calculated height of water and cement inside the casing				
Capacity of cylinder 9.625"	46.94	l/m		
Capacity of anchor casing 9.625"	56797.40	l	56.80	m3
Volume of slurry	53296.00	l	53.30	m3
60% freshwater	31977.60	l	31.98	m3
40% cement (class G)	21318.40	l	21.32	m3

TABLE 7: Results of collapse pressure calculations for each casing

<b>Surface casing</b>				
<i>Collapse pressure during running of the casing</i>				
<i>Collapse at surface</i>	0	bar	0	psi
<i>Collapse at shoe</i>	9.42	bar	136.59	psi
Collapse at shoe by safety factor 1.2	11.30	bar	163.91	psi
Pe at shoe	9.42	bar	136.59	psi
Pi at shoe	0	bar	0	psi
<i>Collapse pressure after running the casing</i>				
<i>Collapse at surface</i>	0	bar	0	psi
<i>Collapse at shoe</i>	14.13	bar	204.89	psi
Collapse at shoe by safety factor 1.2	16.95	bar	245.87	psi
Pe at shoe	29.82	bar	432.54	psi
Pi at shoe	15.70	bar	227.65	psi
<b>Anchor casing</b>				
<i>Collapse pressure during running of the casing</i>				
<i>Collapse at surface</i>	0	bar	0	psi
<i>Collapse at shoe</i>	49.44	bar	717.11	psi
Collapse at shoe by safety factor 1.2	59.33	bar	860.54	psi
Pe at shoe	49.44	bar	717.11	psi
Pi at shoe	0	bar	0	psi
<i>Collapse pressure after running the casing</i>				
<i>Collapse at surface</i>	0	bar	0	psi
<i>Collapse at shoe</i>	42.38	bar	614.67	psi
Collapse at shoe by safety factor 1.2	50.86	bar	737.60	psi
Pe at shoe	89.47	bar	1297.63	psi
Pi at shoe	47.09	bar	682.96	psi

TABLE 7 cont.: Results of collapse pressure calculations for each casing

<b>Production casing</b>				
<i>Collapse pressure during running the casing</i>				
<i>Collapse at surface</i>	0	bar	0	psi
<i>Collapse at shoe</i>	124.64	bar	1807.72	psi
Collapse at shoe by safety factor 1.2	149.56	bar	2169.27	psi
Pe at shoe	124.64	bar	1807.72	psi
Pi at shoe	0	bar	0	psi
<i>Collapse pressure after running the casing</i>				
<i>Collapse at surface</i>	0	bar	0	psi
<i>Collapse at shoe</i>	106.83	bar	1549.48	psi
<i>Collapse at shoe by safety factor 1.2</i>	128.20	bar	1859.37	psi
Pe at shoe	225.53	bar	3271.11	psi
Pi at shoe	118.70	bar	1721.64	psi

For hydrostatic pressure at each section see Section 6, Table 10

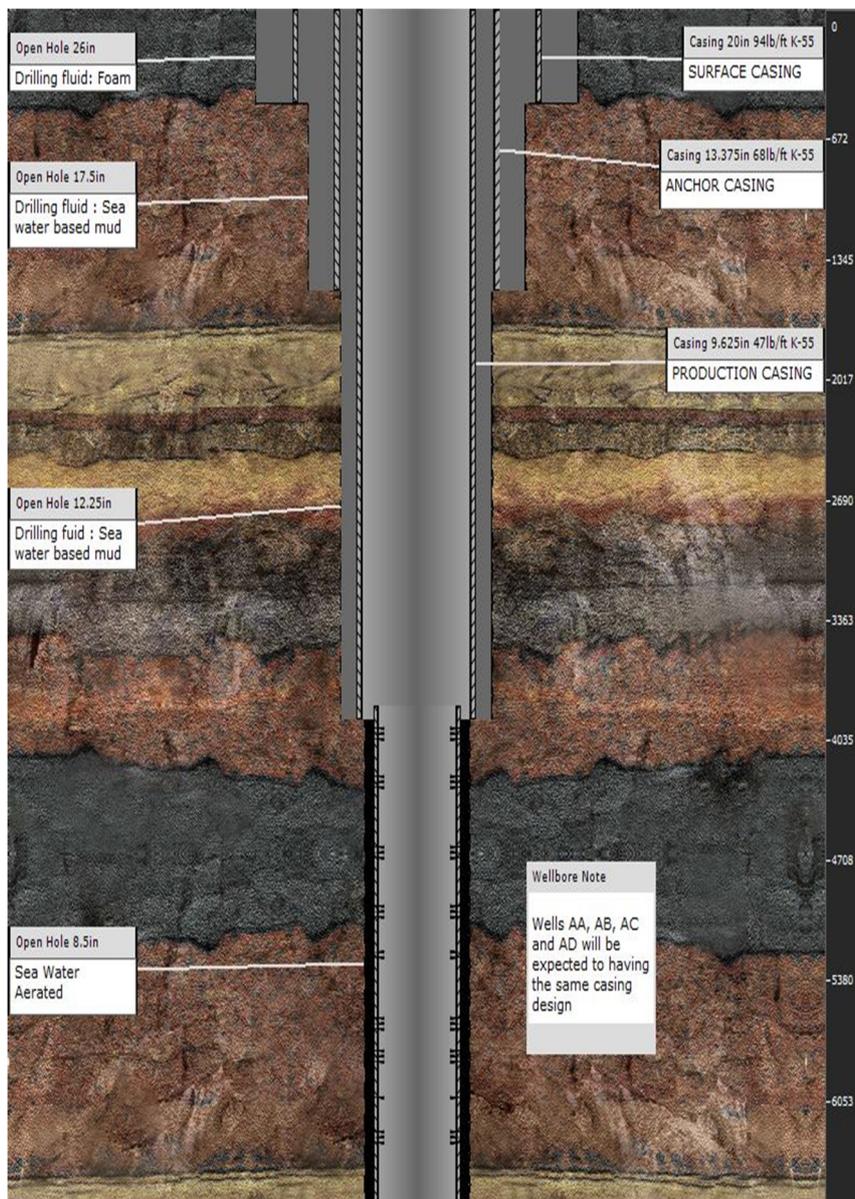


FIGURE 8 : Wellbore schematic, Fiale area

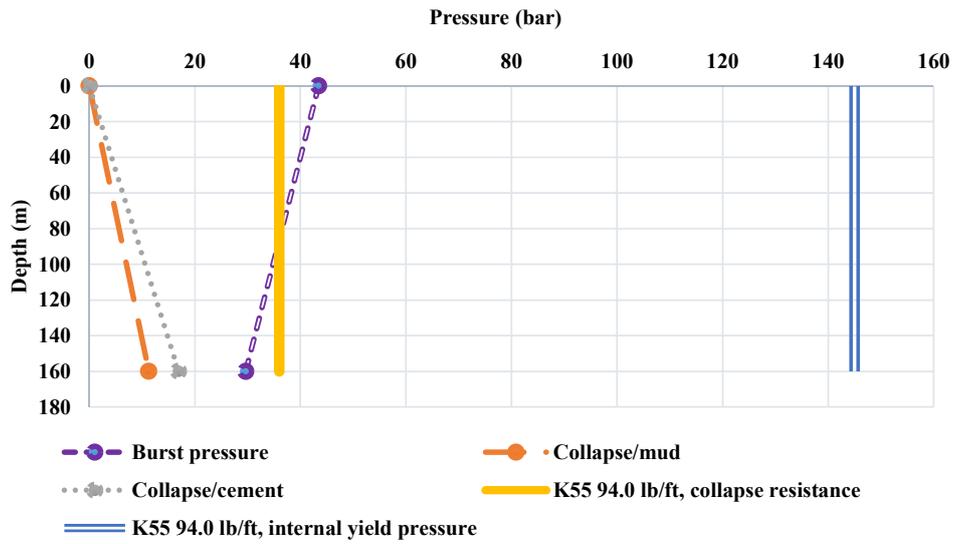


FIGURE 9: 20" casing design

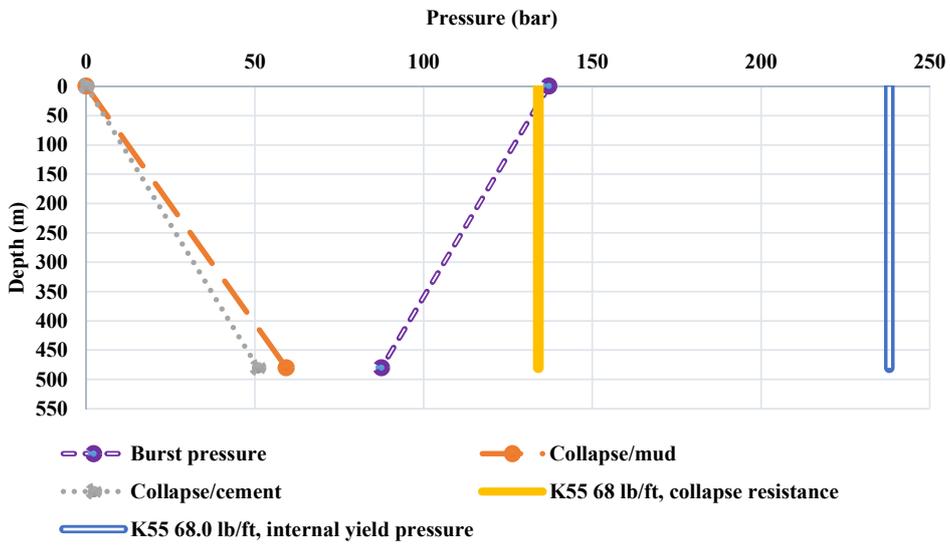


FIGURE 10: 13 3/8" casing design

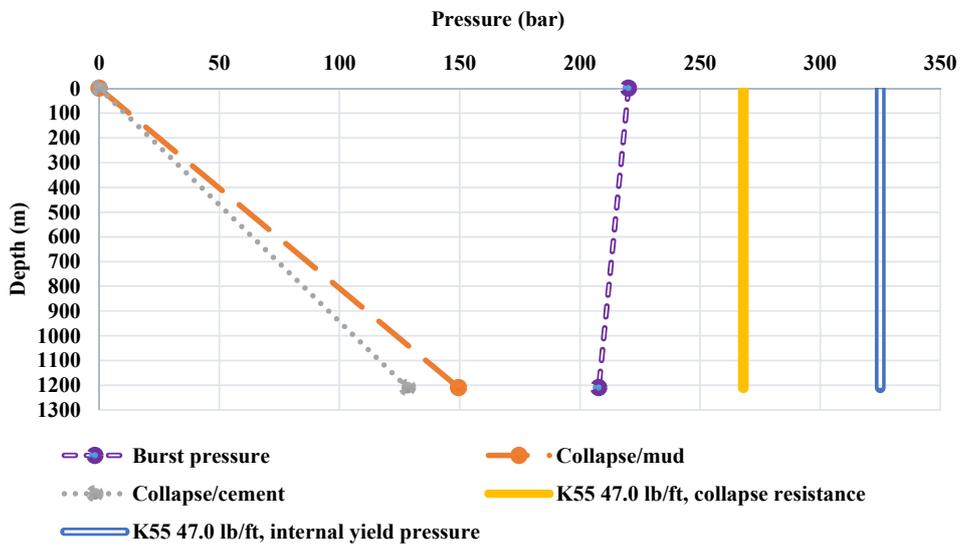


FIGURE 11: 9 5/8" casing design

#### 4.4 Casing design in deviated Wells AA, AB, AC and AD

From the sections above, the general method for casing design was applied to directional wells by simply converting the measured depth (MD) to true vertical depth. The collapse, burst and tension criteria were then applied and the appropriate casing grades were selected. Finally, in the deviated sections of the well, the vertical lengths of selected grades were converted to the measured depth (MD) lengths by simply dividing the vertical depth by  $\cos(\text{angle of deviation})$  (see Appendix II, which shows the well trajectories).

##### Basic design data:

Kick off point for Wells AA, AB, AC and AD = 480 m;

Deviation angle = 30°;

TVD = 2050 m; and

Measured depth (MD) = 2250 m.

The selection of grade and weight provides the basis for checking for tension. The tensile loads are to be included in the design of the casings string. In Table 8, the total tensile load and the safety factor for each section were determined to assure that the safety factor for the tension loads was equal or above 1.5 – 1.8. The entire volume of cement is outside the casing and the casing inside is full of displacement fluid. When the casing is cemented, the effects of shock loading disappear; therefore, a safety factor of 1.4 in tension in the production section could be tolerated. Table 9 shows the compressive loads on the casing due to thermal expansion during heat-up.

TABLE 8: Tensile loads

Selected grade and weight	Max. buoyant weight in 1000 daN	Bending force in 1000 daN	Shock load in 1000 daN	Lifting force due to wellhead pressure in 1000 daN	Force due to pressure testing in 1000 daN	Total tensile load in 1000 daN	Safety factor
Surface casing 20" 94.0 lb/ft K55	19.2		133.8		161.3	314.1	2.1
Anchor casing 13.375" 68.0 lb/ft K55	41.6		96.8	36.4	125.84	300.2	1.6
Production casing 9.625" 47.0 lb/ft K55	72.5	31.71	66.9		68.8	239.9	1.4

TABLE 9: Compressive loads due to thermal expansion during heating-up

	Surface casing	Anchor casing	Production casing
Compressive loads in 1000 daN	156	352	508

Biaxial correction is resolved using an equation from the *Viking Engineering* programme (Appendix IV) for reducing the collapse rating in the presence of axial tension. The collapse resistance of the casing in the presence of axial stress is calculated by reducing the yield strength in accordance to the axial stress, giving:

*Surface casing: 20 " 94.0 lb/ft K55*

Axial stress = 1599.5 psi

Reduced yield strength due to axial stress: 54.2 ksi

Reduced collapse pressure: 520 psi

*Anchor casing: 13.375 " 54.50 lb/ft K55*

Axial stress = 4804.4 psi

Reduced yield strength due to axial stress: 52.4 ksi

Reduced collapse pressure: 1900 psi

Production casing: 9.625 " 40 lb/ft K55

Axial stress = 11096 psi

Reduced yield strength due to axial stress: 48.6ksi

Reduced collapse pressure: 3600 psi.

## 5. CEMENTING PROCESS

In this section, the cement job for each casing will be calculated. The casings of Wells AA, AB, AC, and AD will be cemented in place with a single-stage cementing operation with a cementing head (single-stage cementing), which is the most common type of cementing operation when there is no loss of circulation (Bett, 2010). Other common cementing methods in geothermal wells can be used such as multiple-stage and inner-string cementing. The single-stage procedure follows the following steps (Figure 12):

- Installation of the cementing head;
- Cleaning out the mud in the annulus;
- Release wiper plug, to clean the inside of the casing and to maintain the spacer front;
- Pump spacer into the casing;
- Pump cement;
- Release shut-off plug; and
- Stop the displacement process when the plug reaches the float collar.

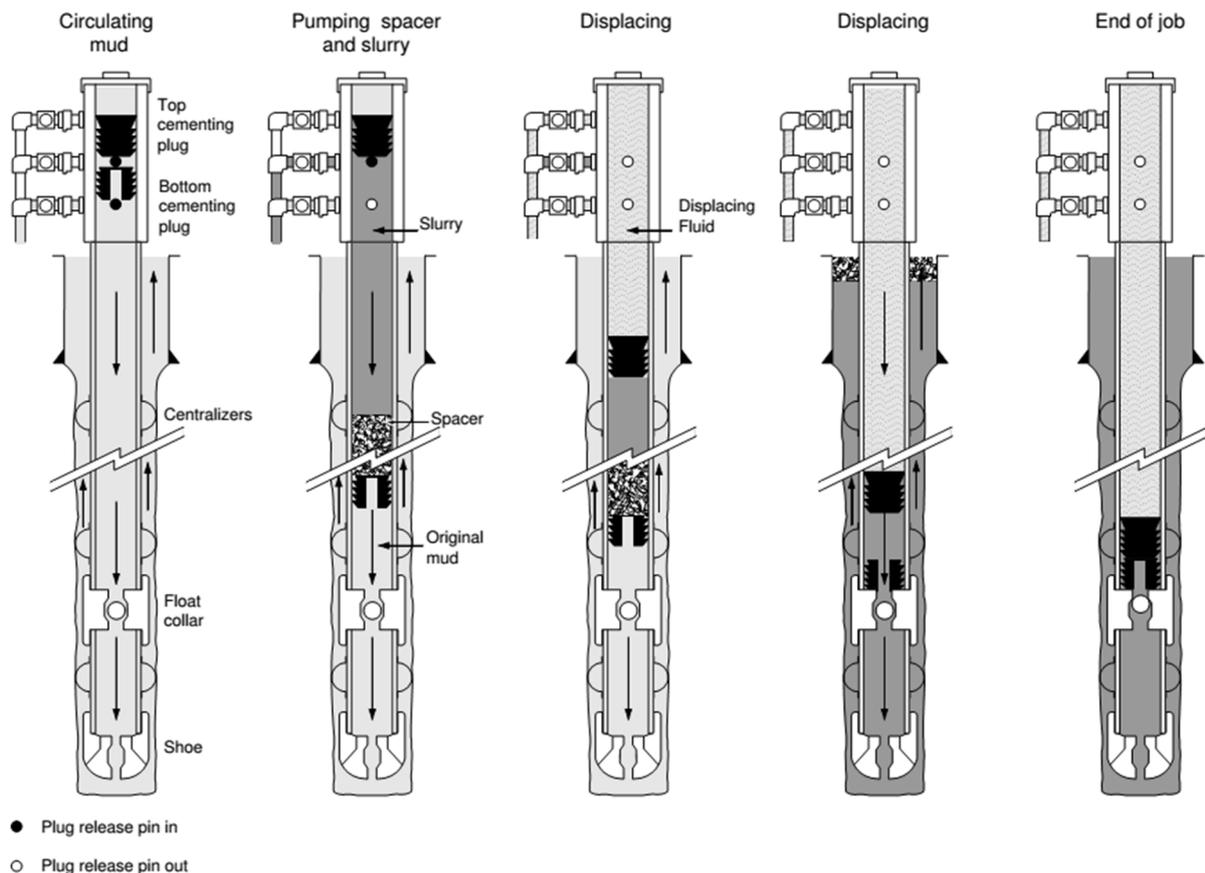


FIGURE 12: Single-stage cementing operation

### 5.1 Cementing calculations for Asal Wells AA, AB, AC and AD

All casings are fully cemented back to the surface. For each casing, the total slurry volume is the sum of four volumes: slurry volume between the casing and the open hole, slurry volume left inside the casing below the float collar, slurry volume in the rathole, and slurry volume in the annulus between the casing and the previous casing (Figure 12). The duration of the operation can be calculated using a displacement rate of 24 l/s and a mixing and pumping rate of 20 l/s (Thórhallsson, 2013).

*Conductor casing, 30"*

V = Volume of an annular space between open hole (28") and conductor casing:

Slurry	0.4	m <sup>3</sup>
Plus 60% excess	0.64	m <sup>3</sup>

*Surface casing: 20" 94.0 lb/ft K55*

<u>Casing 20" 94.0 lb/ft K55</u>		<u>Open hole 26"</u>	
Capacity	185.32 l/m	Capacity	342.5 l/m
Displacement	202.68 l/m	Depth of open hole	156 m
CSD	160 m		

<u>Previous casing 30"</u>		<u>Rathole</u>	
Capacity	456 l/m	Depth of rathole	2 m
Previous CSD	2 m	Capacity	342.5 l/m

- Slurry volume between casing and hole:  
 $V1 = \text{Depth of open hole} \times (\text{Capacity of open hole (26")} - \text{Casing displacement (20")}) = 22 \text{ m}^3$ .  
 Assume gauge hole, add 60% excess in open hole,  $V1 = 35 \text{ m}^3$ .
- Slurry volume in the rathole:  
 $V2 = \text{Depth of rathole} \times \text{Capacity of open hole (26")} = 0.7 \text{ m}^3$ .  
 Assume gauge hole, add 60% excess in open hole,  $V2 = 1.1 \text{ m}^3$ .
- Slurry volume below the float collar, shoe track:  
 $V3 = \text{Depth of shoe track}$   
 $(10 \text{ m}) \times \text{Casing capacity (20")} = 1.85 \text{ m}^3$ .
- Slurry volume between casing:  
 $V4 = \text{Depth of previous casing} \times (\text{Casing capacity 26"} - \text{Casing displacement 20"}) = 0.51 \text{ m}^3$ .

The total cement required for the surface casing is 38.8 m<sup>3</sup>. The duration of the cementing operation is given by:

$$\text{Duration} = \frac{\text{Slurry volume}}{\text{Pumping and mixing rate}} + \frac{\text{Displacement volume}}{\text{Displacement rate}} + \text{Contingency (1hr)} \quad (44)$$

The displacement volume is the slurry volume inside the casing between the cementing head and the float collar. Therefore, the displacement volume is calculated from the volumetric capacity of the casing and the depth of the float collar in the casing (volumetric capacity of casing  $\times$  depth of float collar).

- Displacement volume =  $(150+12 \text{ (depth landing joint)}) \times 185.32 \text{ l/m} = 30.02 \text{ m}^3$ .
- Duration of operation = 113 minutes.

*Anchor casing: 13.375" 54.50 lb/ft K55*

<u>Casing 13.375" 68.0 lb/ft K55</u>	<u>Open hole 17.5"</u>
Capacity 78.1 l/m	Capacity 155.2 l/m
Displacement 90.65 l/m	Depth of open hole 318 m
CSD 480 m	

<u>Previous casing 20"</u>	<u>Rathole</u>
Capacity 185.32 l/m	Depth of rathole 2 m
Displacement 202.68 l/m	Capacity 155.2 l/m
Previous CSD 160 m	

- Slurry volume between casing and open hole:  
 $V1 = \text{Depth of open hole} \times (\text{Capacity open hole (17.5")} - \text{Casing displacement (13.375)}) = 21 \text{ m}^3$ .  
 Assume gauge hole, add 60% excess in open hole,  $V1 = 33 \text{ m}^3$ .
- Slurry volume in the rathole:  
 $V2 = \text{Depth of rathole} \times \text{Capacity of open hole (17.5")} = 0.3 \text{ m}^3$ .  
 Assume gauge hole, add 60% excess in open hole,  $V2 = 0.5 \text{ m}^3$ .
- Slurry volume below the float collar, shoe track:  
 $V3 = \text{Depth of shoe track (10 m)} \times \text{Casing capacity (13.375")} = 0.78 \text{ m}^3$ .
- Slurry volume between casing:  
 $V4 = \text{Depth of previous casing} \times (\text{Casing capacity 20"} - \text{Casing displacement 13.375"}) = 15.15 \text{ m}^3$ .  
 The total cement required for the anchor casing is  $49.5 \text{ m}^3$ .
- Displacement volume =  $(470+12 \text{ (depth landing joint)}) \times 78.1 \text{ l/m} = 37.64 \text{ m}^3$ .
- Duration of operation = 127 minutes.

*Production casing 9.625" 47 lb/ft K55*

<u>Casing 9.625" 68.0 lb/ft K55</u>	<u>Open hole 12.25"</u>
Capacity 38.19 l/m	Capacity 76.04 l/m
Displacement 46.94 l/m	Depth of open hole 808 m
CSD (=length) 1290 m	

<u>Previous casing 13.375"</u>	<u>Rathole</u>
Capacity 78.1 l/m	Depth of rathole 2 m
Displacement 90.65 l/m	Capacity 76.04 l/m
Previous CSD 480 m	

- Slurry volume between casing and open hole:  
 $V1 = \text{Depth of open hole} \times (\text{capacity of open hole (12.25")} - \text{casing displacement (9.625)}) = 24 \text{ m}^3$ .  
 Assume gauge hole, add 60% excess in open hole,  $V1 = 38 \text{ m}^3$ .
- Slurry volume in the rathole:  
 $V2 = \text{Depth of rathole} \times \text{capacity of open hole (12.25")} = 0.15 \text{ m}^3$ .  
 Assume gauge hole, add 60% excess in open hole,  $V2 = 0.24 \text{ m}^3$ .
- Slurry volume below the float collar, shoe track:  
 $V3 = \text{Depth of shoe track (10 m)} \times \text{casing capacity (9.625")} = 0.4 \text{ m}^3$ .
- Slurry volume between casing:  
 $V4 = \text{Depth of previous casing} \times (\text{casing capacity 13.375"} - \text{casing displacement 9.625"}) = 15 \text{ m}^3$ .  
 The total cement required for production casing is  $53 \text{ m}^3$ .
- Displacement volume =  $(1280+12 \text{ (depth landing joint)}) \times 38.19 \text{ l/m} = 49 \text{ m}^3$ .
- Duration of operation = 139 minutes.

### 6. WELLHEAD DESIGN

Wellheads include several pieces of equipment; the most important is the master valve which is used to isolate the well. Other equipment include the casing head flange, gaskets, bolts, kill valves and the expansion spool. A typical permanent wellhead can be seen in Figure 13. Wellhead pressure (WHP) can be proportional to the reservoir pressure; when the reservoir pressure is high, the wellhead pressure will likely also be high. The phases of the fluid at the wellhead vary. There can be different phases: saturated water, saturated steam, or gas that accumulates in the well when it is shut in. The surface conditions are never equal to the bottom hole conditions due to the column of the fluid in the well but in some cases, they can be similar. The different wellhead components should be designed to withstand the maximum pressure and temperature exposure under static and flowing conditions. The wellhead should be designed according to the practice codes. The master valve is often chosen by using pressure ratings of flanges, conforming to ANSI b16.5 and to API 6A (Hole, 1996). The top section of the anchor casing, from the surface to around 25 m depth, should also comply with the ASME B31.1 Power piping code.

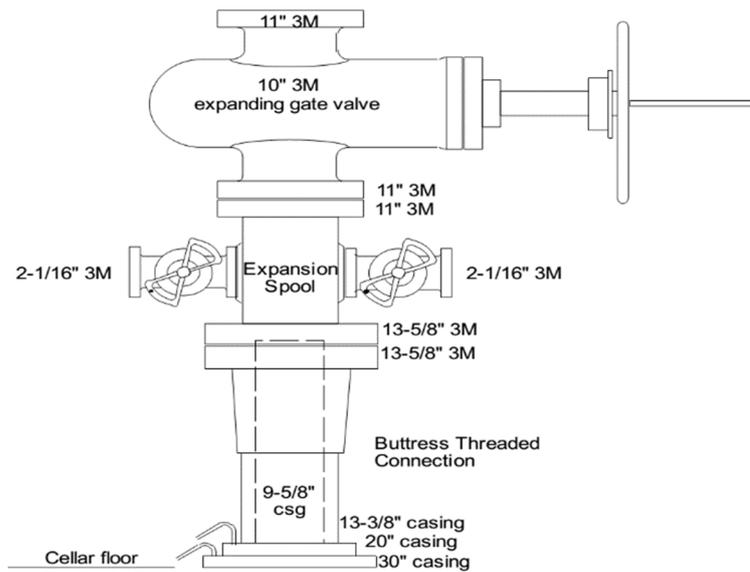


FIGURE 13: Typical complete wellhead

#### 6.1 Wellhead pressure estimate and class

In Table 10, the wellhead pressure is calculated using the density of the saturated liquid. Then one can calculate the hydrostatic pressure and the density of saturated steam in order to calculate the pressure of the steam column in the production section back to the surface and the wellhead. First the hydrostatic pressure is calculated from 200 m (water level) to the bottom of the well at 2000 m at every 50 m. Secondly, the boiling point (1100 m) is determined. From this point, the pressure of the steam column in the production section and to the surface and the wellhead is calculated. The class of the wellhead shall be API 3000; it was chosen by using the pressure ratings of flanges conforming to ANSI b16.5 and to API 6A (Figure 14).

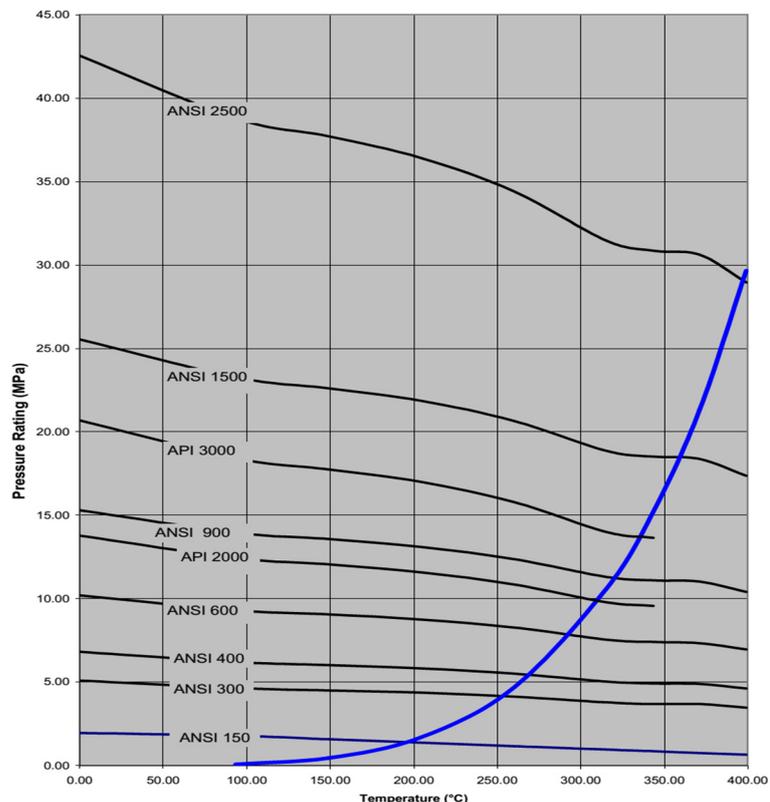


FIGURE 14: Pressure rating of wellhead

TABLE 10: Wellhead pressure estimate

Vertical depth	Temp	Boiling Point	Density		Hydrostatic pressure	Steam column production-section
			Sat. liquid	Sat. vapour		
(m)	(°C)	(bar)	(kg/m <sup>3</sup> )	(kg/m <sup>3</sup> )	(bar)	(bar)
0.0	0.0					<b>94.585</b>
50.0	0.0					94.863
100.0	0.0					95.140
150.0	0.0					95.417
<b>200.0</b>	40.0	0.1	992.2	0.1		95.694
250.0	50.0	0.1	988.0	0.1	4.8	95.971
300.0	60.0	0.2	983.2	0.1	9.7	96.248
350.0	70.0	0.3	977.7	0.2	14.5	96.525
400.0	80.0	0.5	971.8	0.3	19.2	96.802
450.0	90.0	0.7	965.3	0.4	24.0	97.079
500.0	96.4	0.9	960.9	0.5	28.7	97.356
550.0	102.9	1.1	956.3	0.7	33.4	97.634
600.0	109.3	1.4	951.5	0.8	38.0	97.911
650.0	115.7	1.7	946.5	1.0	42.7	98.188
700.0	122.1	2.1	941.4	1.2	47.3	98.465
750.0	128.6	2.6	936.0	1.4	51.9	98.742
800.0	135.0	3.1	930.5	1.7	56.5	99.019
850.0	141.4	3.8	924.9	2.0	61.0	99.296
900.0	147.9	4.5	919.0	2.4	65.5	99.573
950.0	154.3	5.3	913.0	2.8	70.0	99.850
1000.0	160.7	6.3	906.8	3.3	74.4	100.127
1050.0	167.1	7.4	900.4	3.9	78.8	100.405
1100.0	173.6	8.6	893.8	4.5	83.2	100.682
1150.0	170.0	7.9	897.5	4.1	87.6	100.959
1200.0	177.9	9.6	889.2	4.9	92.0	101.236
1250.0	185.8	11.4	880.7	5.8	96.3	<b>101.513</b>
1300.0	193.7	13.6	871.9	6.9	100.6	
1350.0	201.6	16.1	862.8	8.1	104.8	
1400.0	209.5	18.9	853.4	9.5	109.0	
1450.0	217.4	22.0	843.6	11.0	113.1	
1500.0	225.3	25.6	833.4	12.8	117.2	
1550.0	233.2	29.6	822.9	14.8	121.3	
1600.0	241.1	34.1	811.9	17.1	125.2	
1650.0	248.9	39.1	800.4	19.6	129.2	
1700.0	256.8	44.6	788.5	22.5	133.0	
1750.0	264.7	50.6	776.1	25.7	136.8	
1800.0	272.6	57.3	763.0	29.3	140.6	
1850.0	280.5	64.7	749.3	33.5	144.3	
1900.0	288.4	72.7	734.9	38.1	147.9	
1950.0	296.3	81.5	719.6	43.4	151.4	
2000.0	304.2	91.1	703.3	49.5	154.8	
<b>2050.0</b>	<b>312.11</b>	<b>101.513</b>	<b>685.892</b>	<b>56.494</b>	<b>158.212</b>	

## 7. CONCLUSIONS

The casing programme is vital to the success and safety of the well drilling process and to the integrity and life of the well. The design of Wells AA, AB, AC and AD was oversized to avoid any risk. After drilling the first well, the first useful geotechnical data for the new drilling site will be available; then the design of the other three wells can be optimized.

Generally, drilling can be done with foam or mud. The choice of drilling fluid will depend on the geology and the surrounding terrain. In the Fiale area, it is most likely that the drilling fluid used will consist of seawater based drilling mud. But in the production section, using aerated drilling should be considered because of possible low permeability.

## ACKNOWLEDGEMENTS

I would first like to thank my supervisor, Arnar Bjarki Árnason, for teaching me to be more independent throughout this project. I also would like to thank my teachers at UNU-GTP.

I especially want to thank Mr. Ingimar Gudni Haraldsson, Ms. Málfrídur Ómarsdóttir, Mr. Markús A. G. Wilde and Ms. Thórhildur Ísberg, all of whom dedicated their time to me during my stay in Iceland. Finally, I express my sincere gratefulness to the now retired director, Dr. Ingvar Birgir Fridleifsson, and the new director, Mr. Lúdvík S. Georgsson.

## REFERENCES

Aquater, 1989: *Asal 5 well report - final report*. Aquater, Italy, 64 pp.

Árnason, K., Björnsson, G., Flóvenz, Ó.G., Haraldsson, E.H., 1988: *Geothermal resistivity survey in the Asal rift, volume 1: Main text*. Orkustofnun, Reykjavík, OS-88031/JHD-05, prepared for the UND-OPS and ISERST, 48 pp.

Baker Hughes INTEQ, 1995: *Drilling engineering workbook. A distributed learning course*. Baker Hughes INTEQ Inc., 410 pp.

Bett, E.K., 2010: Geothermal well cementing, materials and placement techniques. Report 10 in: *Geothermal training in Iceland 2010*. UNU-GTP, Iceland, 99-130.

BG Group, 2001: *Well engineering and production operations management system – Casing design manual*. B.G. Group, document number WSD CD 01, 51 pp.

Devereux, S., 1998: *Practical well planning and drilling*. Pennwell, Oklahoma, OK, United States 524 pp.

Elmi, H.D., 2005: Analysis of geothermal well test data from the Asal rift area, Republic of Djibouti. Report 6 in: *Geothermal training in Iceland 2005*. UNU-GTP, Iceland, 39-59.

Gabolde G., and Nguyen, J.P., 2006: *Drilling data handbook* (8<sup>th</sup> edition). Institut Française du Petrole Publications, Paris, 552 pp.

Heriot-Watt University, 2010: *Drilling engineering*. Heriot-Watt University, Department of petroleum engineering, 539 pp.

Hole, H.M., 1996: Geothermal Energy New Zealand, Ltd. *Seminar on Geothermal Drilling Engineering, Jakarta, Indonesia, Seminar handbook.*

Hosseini-Pourazad, H., 2005: High-temperature geothermal well design. Report 9 in: *Geothermal training in Iceland 2005.* UNU-GTP, Iceland, 111-123.

Jalludin, M., 2010: State of knowledge of the geothermal provinces of the Republic of Djibouti. *Paper presented at "Short Course V on Exploration for Geothermal Resources" organized by UNU-GTP, KenGen and GDC, Lake Naivasha, Kenya,* 14 pp.

Khairah, A.E., 1989: *Borehole geology of well Asal-5, Asal geothermal field, Djibouti.* UNU-GTP, Iceland, report 6, 31 pp.

Meinken, W., and Schülein, S., 2012: *Geothermal resources evaluation project Djibouti, environmental and social impacts.* Fichtner GmbH and Co., final report, 14 pp.

NZS, 1991: *Code of practice for deep geothermal wells.* Standards New Zealand, NZS 2403:1991, 96 pp.

Rabia, H., 1987: *Fundamentals of casing design, vol. 1.* Graham & Trotham, London, United Kingdom, 285 pp.

REI, 2008: *Drilling and testing of geothermal exploration wells in the Asal area, Djibouti: Environmental management plan.* Reykjavik Energy Invest, report REI-2008/Assal 1, 58 pp.

Saemundsson, K., 1988: *Djibouti geothermal project. Analysis of geological data pertaining to geothermal exploration of Asal rift.* United Nations Development Programme, 18 pp.

Stiltjes, L., 1976: Research for a geothermal field in a zone of oceanic spreading: Examples of the Asal Rift. *Proceedings of the 2<sup>nd</sup> UN Symposium on the Development and Use of Geothermal Resources, San Francisco, CA, United States, 1,* 613-623.

Thórhallsson, S., 2013: *Geothermal drilling technology.* UNU-GTP, Iceland, unpublished lecture notes.

Varet, J., 1978: Geology of central and southern Afar (Ethiopia and Djibouti Republic). Centre National de la Recherche Scientifique, Paris, France, 124 pp.

Virkir-Orkint, 1990: *Djibouti, geothermal scaling and corrosion study.* Virkir-Orkint, Reykjavík, report, 109 pp.

## APPENDIX I: API specifications, standards and bulletins

**API SPEC 5CT**, "Specification for casing and tubing": Covers seamless and welded casing and tubing, couplings, pup joints and connectors in all grades. Processes of manufacture, chemical and mechanical property requirements, methods of test and dimensions are included.

**API STD 5B**, "Specification for threading, gauging, and thread inspection for casing, tubing, and line pipe threads": Covers dimensional requirements on threads and thread gauges, stipulations on gauging practice, gauge specifications and certifications, as well as instruments and methods for the inspection of threads of round-thread casing and tubing, buttress thread casing, and extreme-line casing and drill pipe.

**API RP 5A5**, “Recommended practice for filed inspection of new casing, tubing and plain-end drill pipe”: Provides a uniform method of inspecting tubular goods.

**API RP 5B1**, “Recommended practice for thread inspection on casing, tubing and line pipe”: The purpose of this recommended practice is to provide guidance and instructions on the correct use of thread inspection techniques and equipment.

**API RP 5C1**, “Recommended practice for care and use of casing and tubing”: Covers use, transportation, storage, handling, and reconditioning of casing and tubing.

**API RP5C5**, “Recommended practice for evaluation procedures for casing and tubing connections”: Describes tests to be performed to determine the galling tendency, sealing performance and structural integrity of tubular connections.

**API BULL 5A2**, “Bulletin on thread compounds”: Provides material requirements and performance tests for two grades of thread compound for use on oil-field tubular goods.

**API BULL 5C2**, “Bulletin on performance properties of casing and tubing”: Covers collapsing pressures, internal yield pressures and joint strengths of casing and tubing and minimum yield load for drill pipe.

**API BULL 5C3**, “Bulletin on formulas and calculations for casing, tubing, drill pipe and line pipe properties”: Provides formulas used in the calculations of various pipe properties, also background information regarding their development and use.

**API BULL 5C4**, “Bulletin on round thread casing joint strength with combined internal pressure and bending.” Provides joint strength of round thread casing when subject to combined bending and internal pressure.

## APPENDIX II: Calculated hole trajectories for Wells AA, AB, AC and AD

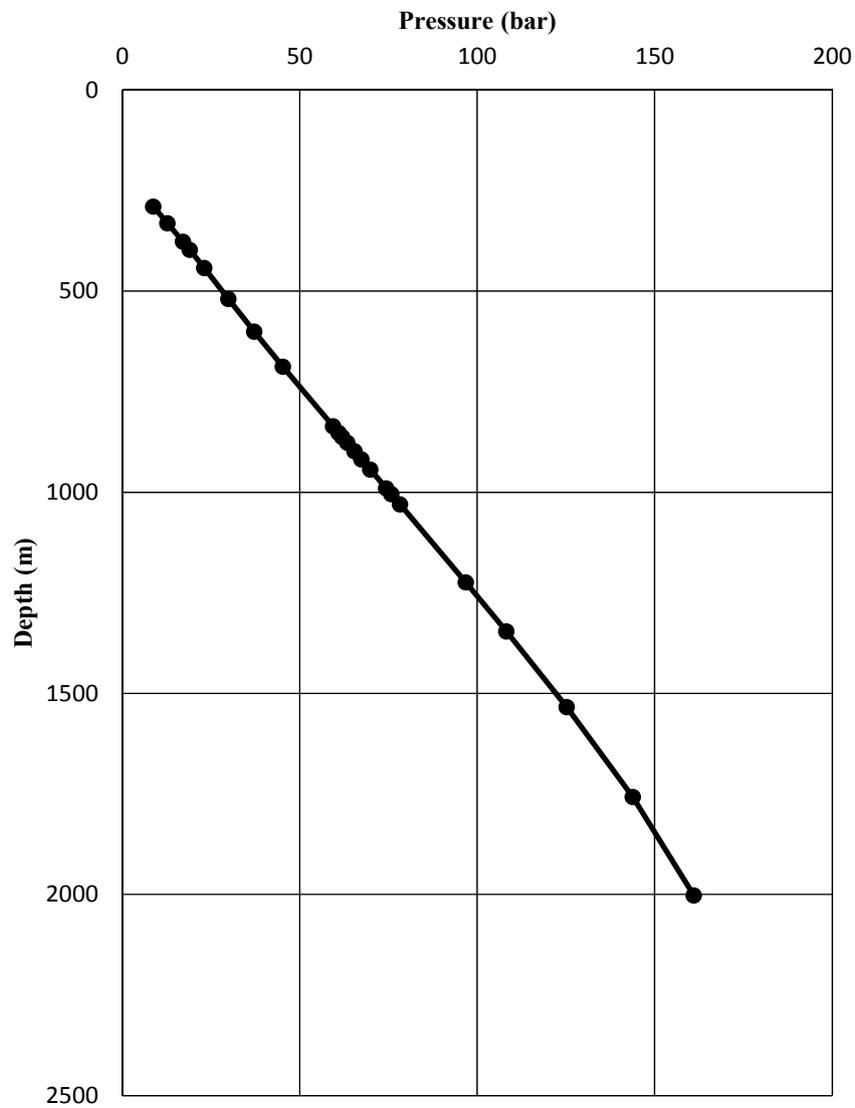
Dogleg severity: 2.5 degrees/30 ft., Deviation angle 30 degrees

MD (m)	Inclination (°)	TVD (m)	Displacement (m)
0	0	0	0
30	0	30	0
60	0	60	0
90	0	90	0
120	0	120	0
150	0	150	0
160	0	160	0
180	0	180	0
210	0	210	0
240	0	240	0
270	0	270	0
300	0	300	0
330	0	330	0
360	0	360	0
390	0	390	0
420	0	420	0
450	0	450	0
480	0	480	0

<b>MD (m)</b>	<b>Inclination (°)</b>	<b>TVD (m)</b>	<b>Displacement (m)</b>
510	2.5	510.0	0.7
540	5	539.9	2.6
570	7.5	569.8	5.9
600	10	599.4	10.4
630	12.5	628.8	16.3
660	15	658.0	23.4
690	17.5	686.8	31.8
720	20	715.2	41.5
750	22.5	743.1	52.3
780	25	770.6	64.4
810	27.5	797.5	77.7
840	30	823.8	92.1
870	30	849.8	107.1
900	30	875.8	122.1
930	30	901.7	137.1
960	30	927.7	152.1
990	30	953.7	167.1
1020	30	979.7	182.1
1050	30	1005.7	197.1
1080	30	1031.6	212.1
1110	30	1057.6	227.1
1140	30	1083.6	242.1
1170	30	1109.6	257.1
1200	30	1135.6	272.1
1230	30	1161.6	287.1
1260	30	1187.5	302.1
1290	30	1213.5	317.1
1320	30	1239.5	332.1
1350	30	1265.5	347.1
1380	30	1291.5	362.1
1410	30	1317.4	377.1
1440	30	1343.4	392.1
1470	30	1369.4	407.1
1500	30	1395.4	422.1
1530	30	1421.4	437.1
1560	30	1447.3	452.1
1590	30	1473.3	467.1
1620	30	1499.3	482.1
1650	30	1525.3	497.1
1680	30	1551.3	512.1
1710	30	1577.2	527.1
1740	30	1603.2	542.1
1770	30	1629.2	557.1
1800	30	1655.2	572.1
1830	30	1681.2	587.1
1860	30	1707.1	602.1
1890	30	1733.1	617.1
1920	30	1759.1	632.1
1950	30	1785.1	647.1
1980	30	1811.1	662.1
2010	30	1837.1	677.1
2040	30	1863.0	692.1

MD (m)	Inclination (°)	TVD (m)	Displacement (m)
2070	30	1889.0	707.1
2100	30	1915.0	722.1
2130	30	1941.0	737.1
2160	30	1967.0	752.1
2190	30	1992.9	767.1
2220	30	2018.9	782.1
2250	30	2050	797.1

**APPENDIX III: Hydrostatic pressure in Well Asal 5**



**APPENDIX IV: Reduced collapse resistance, production casing**

		
API Collapse		
<b>Input</b>		
D (in)	9,625	Pipe Outside Diameter
Weight (lbf/ft)	47	Pipe Weight Per Foot
Grade	K55	Pipe Grade
Yield Strength (ksi)	48,6	Pipe Yield Strength
Wall (in)	0,472	Pipe Wall Thickness
Nominal ID (in)	8,681	Nominal Inside Diameter
Collapse Resistance (psi)	3600	Calculated Collapse Rating
Collapse Calculations		
D/t	20,39	
A	2,970661	
B	0,050525	
C	995,6239	
F	2,011316	
G	0,034209	
Yield Strength Collapse (psi)	4480	Collapse Ratings Based on D/t
D/t	15,44	
Plastic Collapse (psi)	3570	Collapse Ratings Based on D/t
D/t	25,89	
Transition Collapse (psi)	3090	Collapse Ratings Based on D/t
D/t	39,53	
Elastic Collapse (psi)	6130	Collapse Ratings Based on D/t
This calculator calculates API collapse resistance for a specific pipe.		